

(12) INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(19) World Intellectual Property  
Organization  
International Bureau



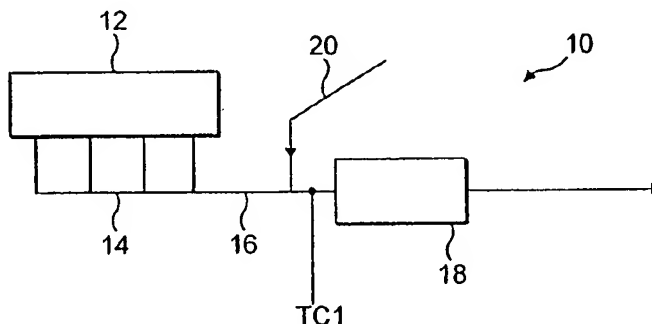
(43) International Publication Date  
29 December 2004 (29.12.2004)

PCT

(10) International Publication Number  
**WO 2004/113691 A2**

- (51) International Patent Classification<sup>7</sup>: **F01N 3/02**,  
3/20, 9/00, 11/00
- (21) International Application Number:  
PCT/GB2004/002643
- (22) International Filing Date: 18 June 2004 (18.06.2004)
- (25) Filing Language: English
- (26) Publication Language: English
- (30) Priority Data:  
0314242.9 18 June 2003 (18.06.2003) GB  
0314463.1 23 June 2003 (23.06.2003) GB  
0322963.0 1 October 2003 (01.10.2003) GB
- (71) Applicant (for all designated States except US): **JOHN-  
SON MATTHEY PUBLIC LIMITED COMPANY**  
[GB/GB]; 2-4 Cockspur Street, Trafalgar Street, London  
SW1Y 5BQ (GB).
- (72) Inventors; and  
(75) Inventors/Applicants (for US only): **ALLANSSON**,  
Eive, Tord, Ronny [SE/SE]; Norra Annebergsvagen 123,  
S-434 96 Kungsbacka (SE). **ANDREASSON**, Anders,  
Klas [SE/SE]; Traneredsvagen 60A, S-426 77 V Frolunda  
(SE). **GOERSMANN**, Claus, Friedrich [DE/GB]; 39  
Cromwell Road, Cambridge CB1 3EB (GB). **LAVENIUS**,  
Mats [SE/SE]; Vandstensvagen 13, S-433 30 Partille (SE).  
**TWIGG**, Martyn, Vincent [GB/GB]; 108 Ermine Street,  
Caxton, Cambridge CB3 8PQ (GB). **WALKER**, Andrew,
- (81) Designated States (unless otherwise indicated, for every  
kind of national protection available): AF, AG, AI, AM,  
AT, AU, AZ, BA, BB, BG, BR, BW, BY, BZ, CA, CH, CN,  
CO, CR, CU, CZ, DE, DK, DM, DZ, EC, EE, EG, ES, FI,  
GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE,  
KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MA, MD,  
MG, MK, MN, MW, MX, MZ, NA, NI, NO, NZ, OM, PG,  
PH, PL, PT, RO, RU, SC, SD, SE, SG, SK, SL, SY, TJ, TM,  
TN, TR, TT, TZ, UA, UG, US, UZ, VC, VN, YU, ZA, ZM,  
ZW.
- (84) Designated States (unless otherwise indicated, for every  
kind of regional protection available): ARIPO (BW, GH,  
GM, KE, LS, MW, MZ, NA, SD, SL, SZ, TZ, UG, ZM,  
ZW), Eurasian (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM),  
European (AT, BE, BG, CH, CY, CZ, DE, DK, EE, ES, FI,  
FR, GB, GR, HU, IE, IT, LU, MC, NL, PL, PT, RO, SE, SI,  
SK, TR), OAPI (BF, BJ, CF, CG, CI, CM, GA, GN, GQ,  
GW, ML, MR, NE, SN, TD, TG).
- Published:  
— without international search report and to be republished  
upon receipt of that report
- For two-letter codes and other abbreviations, refer to the "Guid-  
ance Notes on Codes and Abbreviations" appearing at the begin-  
ning of each regular issue of the PCT Gazette.

(54) Title: METHODS OF CONTROLLING REDUCTANT ADDITION



(57) Abstract: An exhaust system (10) for a vehicular lean-burn internal combustion engine (12) comprises a NO<sub>x</sub> reduction catalyst (18), a source of reductant, means (20) for contacting the catalyst (18) with the reductant, means (TC1) for sensing the temperature of the exhaust gas and/or the catalyst bed and means, when in use, for controlling reductant addition, wherein the reductant addition control means supplies an amount of reductant to the catalyst at a rate corresponding to a measured temperature value of the exhaust gas and/or catalyst bed, which temperature value has been pre-determined to correlate, in use, with an amount of NO<sub>x</sub> in the exhaust gas.

WO 2004/113691 A2

**METHODS OF CONTROLLING REDUCTANT ADDITION**

5       The present invention relates to methods of controlling reductant addition to catalytically convert NO<sub>x</sub> in exhaust gas of an internal combustion engine to N<sub>2</sub>.

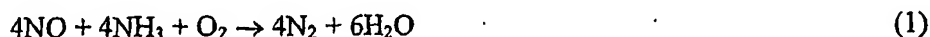
It is known to catalytically reduce NO<sub>x</sub> in exhaust gas of an internal combustion engine to N<sub>2</sub> with a suitable reductant. Three examples are selective catalytic reduction  
10 (SCR), lean-NO<sub>x</sub> catalysis and NO<sub>x</sub>-trap regeneration.

In SCR, the reductant is typically a NO<sub>x</sub>-specific reactant. By "NO<sub>x</sub>-specific reactant" herein, we mean a reducing agent that, in most conditions, preferentially reduces NO<sub>x</sub> over other components of a gaseous mixture. Examples of NO<sub>x</sub>-specific  
15 reactants include nitrogenous compounds such as nitrogen hydrides, e.g. ammonia (NH<sub>3</sub>) or hydrazine as such or by way of a NH<sub>3</sub> precursor.

By "NH<sub>3</sub> precursor" we mean one or more compounds from which NH<sub>3</sub> can be derived, e.g. by hydrolysis. These include urea (CO(NH<sub>2</sub>)<sub>2</sub>) as an aqueous solution or as  
20 a solid or ammonium carbamate (NH<sub>2</sub>COONH<sub>4</sub>). If the urea is used as an aqueous solution, a eutectic mixture, e.g. 32.5% urea (aq), is preferred. Additives can be included in the aqueous solutions to reduce the crystallisation temperature.

Known SCR catalysts include Pt-based catalysts, which can catalyse the  
25 reduction of NO<sub>x</sub> with NH<sub>3</sub> at between about 175°C and about 250°C, medium temperature vanadium-based catalysts e.g. V<sub>2</sub>O<sub>5</sub>/TiO<sub>2</sub>, which operate in the temperature range between about 260°C and about 450°C and zeolite-based catalysts which function with increasing activity at increasing temperature.

30       Several chemical reactions occur in the NH<sub>3</sub> SCR system, all of which represent desirable reactions which reduce NO<sub>x</sub> to elemental nitrogen. The overall desired reaction is represented in equation (1).



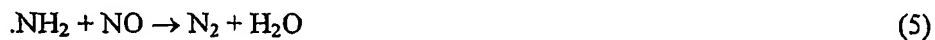
Competing, non-selective reactions with oxygen can produce secondary emissions or may unproductively consume  $\text{NH}_3$ . One such non-selective reaction is the complete oxidation of  $\text{NH}_3$ , represented in equation (2).



It will be appreciated that at lower temperatures, below about 100-200°C,  $\text{NH}_3$  can also react with  $\text{NO}_2$  to produce an explosive mixture of ammonium nitrate ( $\text{NH}_4\text{NO}_3$ ) and ammonium nitrite ( $\text{NH}_4\text{NO}_2$ ). For the avoidance of doubt, the present invention  
10 does not embrace such reactions or the promotion of conditions which bring them about. For example, the reaction can be avoided by ensuring that the temperature does not fall below about 200°C or by supplying into a gas stream less than the precise amount of  $\text{NH}_3$  necessary for the stoichiometric reaction with  $\text{NO}_x$  (1 to 1 mole ratio).

15            Urea hydrolyses at temperatures above 160°C according to equation (3) to liberate  $\text{NH}_3$  itself. It is also believed to decompose thermally at this temperature and above according to equations (4) and (5) resulting in reduction of  $\text{NO}_x$ , as evidenced by formation of CO during SCR processes with urea (see SAE 900496 and SAE 930363 (both incorporated herein by reference)).

20



25            Lean- $\text{NO}_x$  catalysts (LNCs) are sometimes also referred to in the literature as lean- $\text{NO}_x$  reduction catalysts, "DeNOx catalysts" and  $\text{NO}_x$  occluding catalysts.

In lean- $\text{NO}_x$  catalysis, hydrocarbons (HC) react with nitrogen oxides ( $\text{NO}_x$ ), rather than oxygen ( $\text{O}_2$ ), to form nitrogen ( $\text{N}_2$ ), carbon dioxide ( $\text{CO}_2$ ) and water ( $\text{H}_2\text{O}$ )  
30 according to reaction (6).



The competitive, non-selective reaction with oxygen is given by reaction (7).



- 5        There are two preferred groups of LNC to selectively promote the desired reaction (6) described in the literature: platinum (Pt) on alumina ( $\text{Al}_2\text{O}_3$ ) and copper (Cu)-substituted zeolite such as Cu/ZSM-5.

10        A typical  $\text{NO}_x$ -trap formulation includes a catalytic oxidation component, such as Pt, a  $\text{NO}_x$ -storage component, such as compounds of alkali metals e.g. potassium and/or caesium; compounds of alkaline earth metals, such as barium or strontium; or compounds of rare-earth metals, typically lanthanum and/or yttrium; and a reduction catalyst, e.g. rhodium. One mechanism commonly given for  $\text{NO}_x$ -storage during lean engine operation for this formulation is that, in a first step, the nitric oxide reacts with  
15        oxygen on active oxidation sites on the Pt to form  $\text{NO}_2$ . The second step involves adsorption of the  $\text{NO}_2$  by the storage material in the form of an inorganic nitrate.

20        When the engine runs intermittently under enriched conditions or at elevated temperatures, the nitrate species become thermodynamically unstable and decompose, producing NO or  $\text{NO}_2$ . Under rich conditions, these nitrogen oxides are reduced by carbon monoxide, hydrogen and hydrocarbons to  $\text{N}_2$ , which can take place over the reduction catalyst.

25        Whilst the inorganic  $\text{NO}_x$  storage component is typically present as an oxide, it is understood that in the presence of air or exhaust gas containing  $\text{CO}_2$  and  $\text{H}_2\text{O}$  it may also be in the form of the carbonate or possibly the hydroxide. We also explain in our WO 00/21647 (incorporated herein by reference) that  $\text{NO}_x$ -specific reactants can be used to regenerate a  $\text{NO}_x$ -trap.

30        EP-B-0341832 (incorporated herein by reference) describes a process for combusting particulate matter in diesel exhaust gas, which method comprising oxidising nitrogen monoxide in the exhaust gas to nitrogen dioxide on a catalyst, filtering the particulate matter from the exhaust gas and combusting the filtered particulate matter in

the nitrogen dioxide at up to 400°C. Such a system is available from Johnson Matthey and is marketed as the CRT<sup>®</sup>.

5 For the purposes of the present specification, generally we refer to methods of catalytic reduction of NO<sub>x</sub> to N<sub>2</sub> in exhaust gases of internal combustion engines with a suitable reductant as NO<sub>x</sub>-reduction methods and to catalysts for promoting the reduction of NO<sub>x</sub> to N<sub>2</sub> as NO<sub>x</sub>-reduction catalysts. Such catalysts include SCR catalysts, lean-NO<sub>x</sub> catalysts and NO<sub>x</sub>-traps.

10 A problem with the above NO<sub>x</sub> reduction methods is to control the addition of the reductant. If too little reductant is added, NO<sub>x</sub> reduction may be inadequate to meet an emission standard. If too much reductant is added this can cause a number of problems. For example, if the reductant is ammonia, its release into the atmosphere is undesirable because it is a biological poison and it has an unpleasant odour. Whilst excess ammonia  
15 can be oxidised using a suitable catalyst downstream of the NO<sub>x</sub>-reduction catalyst, this produces NO<sub>x</sub>, thus defeating the very purpose of the NO<sub>x</sub> reduction method. Hydrocarbon fuels, e.g. diesel or gasoline, are also legislated components of exhaust gas and so emission of excess hydrocarbon reductant can cause the system to fail a relevant emission standard.

20

Systems to control reductant addition are known, but tend to require very complicated control regimes involving multiple sensor inputs and processors to run complex algorithms. As a result, such systems are very expensive.

25 US-A-2002/0194841 (incorporated herein by reference) discloses a method of reducing NO<sub>x</sub> emissions from vehicular diesel engines by an external reductant supplied to a SCR system including a reducing catalyst, which method comprising the steps of sensing one or more engine operating parameters, such as speed and torque from a speed/load sensor, to predict a concentration of NO<sub>x</sub> emissions indicative of the actual  
30 quantity of NO<sub>x</sub> emissions produced by the engine when the catalyst temperature is within a set range and metering the external reductant to the catalyst at a rate sufficient to cause the catalyst to reduce the calculated concentration of NO<sub>x</sub> emissions.

JP-A-2002-122019 (incorporated herein by reference) discloses a method of preventing thermal degradation in a NO<sub>x</sub>-trap by detecting the temperature in the NO<sub>x</sub>-trap and regulating reductant addition to maintain the NO<sub>x</sub>-trap temperature within a pre-determined range.

5

DE-A-9913268 (incorporated herein by reference) discloses a system for monitoring the efficiency of a NO<sub>x</sub> reduction catalyst in a lean burn engine comprising a fuel feed device for dispensing a predetermined quantity of fuel into exhaust gas upstream of the catalyst to make available an amount of chemical energy and, dependent on catalyst efficiency, to provide an amount of thermal energy, flow and temperature sensors for measuring the thermal energy into and out of the catalyst and a data processing unit communicating with the fuel feed device and the temperature sensors, which constructs an energy balance for the catalyst, and hence provides a correlation signal indicating the performance of the catalyst.

15

In JP-A-62-117620 (incorporated herein by reference), there is described a method removing nitrogen oxides in gasoline engine exhaust gas employing two NO<sub>x</sub>-traps arranged in parallel wherein the NO<sub>x</sub>-traps are used alternately to absorb NO<sub>x</sub> from the exhaust gas under the control of a two-way valve. The off-line NO<sub>x</sub>-trap is regenerated using a suitable reductant such as hydrogen, ammonia, carbon monoxide or methane.

20

"Development and evaluation of a DeNO<sub>x</sub> system based on urea SCR", by Martin Elsener *et al.*, MTZ worldwide, 11/2003, Volume 64, p. 28-31 (incorporated herein by reference) describes the use of a NO<sub>x</sub> sensor which is cross-sensitive against ammonia to provide feedback control of reductant delivery in an exhaust system including a SCR catalyst.

25

We have investigated methods of calibrating reductant addition and of controlling reductant addition by feedback. We have now devised a number of simple methods and systems that are cheap and effective at reducing reductant-based emissions. Systems embodying these methods are particularly relevant to the retrofit market.

30

A first aspect of the invention makes use of only a single temperature measurement, e.g. using a thermocouple, as the control input. Preferably, no reductant is added below a pre-determined temperature because the temperature is too low for the complete NO<sub>x</sub> removal reaction to take place, i.e. reductant addition is controlled so that it is supplied only when the NO<sub>x</sub> reduction catalyst is active. As the load on an engine is increased, the NO<sub>x</sub> level in the exhaust gas increases in a roughly linear fashion. Similarly, the exhaust gas temperature increases with load. We expect, therefore, that for a given engine in a particular application there is a relationship between NO<sub>x</sub> content in the exhaust gas and its temperature. And, that this may approximate to a linear relationship. So, in its simplest form, in this aspect of the invention, the rate of reductant introduced is approximately proportional to the temperature of the exhaust gas. Addition of a reductant in this way provides a very efficient and simple way of maintaining NO<sub>x</sub> reduction on a vehicle. The actual amount of reductant added at different exhaust gas temperatures can depend on the nature of the specific application. However, the trend is for more reductant to remove larger amounts of NO<sub>x</sub> at higher temperatures. In practice a calibration process would determine the exact amounts.

In a system embodiment of the first aspect, the invention provides an exhaust system for a vehicular lean-burn internal combustion engine, which system comprising a catalyst for reducing NO<sub>x</sub> in exhaust gas to N<sub>2</sub> with a suitable reductant, a source of reductant, means for contacting the catalyst with the reductant, means for sensing the temperature of the exhaust gas and/or the catalyst bed and means, when in use, for controlling reductant addition, wherein the reductant addition control means supplies an amount of reductant to the catalyst at a rate corresponding to a measured temperature value of the exhaust gas and/or catalyst bed, which temperature value has been pre-determined to correlate, in use, with an amount of NO<sub>x</sub> in the exhaust gas thereby to promote the reduction of the NO<sub>x</sub>.

In a method embodiment of the first aspect, the invention provides a method of calibrating a rate of reductant addition required to reduce NO<sub>x</sub> in an exhaust gas of a vehicular lean-burn internal combustion engine to N<sub>2</sub> over a suitable catalyst, which method comprising measuring NO<sub>x</sub> in the exhaust gas at a plurality of exhaust gas and/or catalyst bed temperatures and correlating each exhaust gas and/or catalyst bed

temperature value with a rate of reductant addition required to reduce the  $\text{NO}_x$  over the catalyst.

It is known generally in the prior art to determine the temperature of a  $\text{NO}_x$  reduction catalyst and to discontinue addition of reductant when the catalyst temperature is below a pre-determined range to prevent formation of ammonium nitrate and ammonium nitrite and to prevent emissions of reductant at below the catalyst light-off temperature for  $\text{NO}_x$  reduction. The invention of the first aspect is different from this prior art in that the catalyst and/or exhaust gas temperature is used to predict the amount of  $\text{NO}_x$  in the exhaust gas and, accordingly, the rate of reductant addition required to reduce such  $\text{NO}_x$  amount.

A second aspect of the invention provides a simple means of controlling reductant addition by feedback in real-time. In the second aspect, an oxidation catalyst is disposed downstream of the  $\text{NO}_x$  reduction catalyst which is contacted with a reductant. The system is arranged so that the gas is always lean over the oxidation catalyst, e.g. by using secondary addition of air if required. As in the first aspect described above, desirably no reductant is added below a certain critical exhaust gas temperature, at which  $\text{NO}_x$  reduction is ineffective (see hashed line to  $\Delta T$  axis in Fig. 4B). Above this temperature, increasing the amount of reductant causes increasing amounts of  $\text{NO}_x$  in the exhaust gas to be reduced. In practice there is a limit to this effect, and then introducing more reductant fails to enhance  $\text{NO}_x$  reduction (illustrated in Fig 4A). So, there is a region of small excess reductant slip from the  $\text{NO}_x$  reduction catalyst that corresponds to a desirable addition rate above which any more reductant is wasted and can cause failure of a relevant emission standard.

Since the overall gas composition is arranged to be lean, any excess reductant can be oxidised over the downstream oxidation catalyst, and the resulting exotherm may result in a temperature increase across the oxidation catalyst. The inlet temperature to the oxidation catalyst may vary considerably during use, but in this method we are concerned only with the  $\Delta T$  that is a measurement of the excess reductant present. The control strategy (illustrated in Fig. 4B) is based in adjusting the rate of reductant addition to keep the measured  $\Delta T$  within a pre-determined range corresponding to an



optimum NO<sub>x</sub> removal (shaded region in Fig. 4B): reductant addition rate is increased if  $\Delta T$  is too small, or decreased if  $\Delta T$  is larger than desired for optimum efficient NO<sub>x</sub> conversion.

5           According to a system embodiment of the second aspect of the invention, there is provided an exhaust system for a vehicular lean-burn internal combustion engine, which system comprising a catalyst for reducing NO<sub>x</sub> in exhaust gas to N<sub>2</sub> with a suitable reductant, a source of reductant, means for contacting the NO<sub>x</sub> reduction catalyst with the reductant, an oxidation catalyst disposed downstream of the NO<sub>x</sub> reduction catalyst,  
10       means for determining a temperature difference ( $\Delta T$ ) across the oxidation catalyst and means, when in use, for controlling reductant addition, wherein the reductant addition control means controls the rate of reductant addition to maintain  $\Delta T$  within a pre-determined range, wherein the system is configured so that the exhaust gas composition over the oxidation catalyst is lean.

15           A method embodiment of the second aspect of the invention provides a method of controlling, by feedback, addition of reductant to a catalyst suitable for reducing NO<sub>x</sub> in an exhaust gas of a vehicular lean-burn internal combustion engine to N<sub>2</sub>, which method comprising providing an oxidation catalyst for oxidising the reductant  
20       downstream of the NO<sub>x</sub> reduction catalyst, measuring the exhaust gas temperature upstream of the oxidation catalyst, measuring the exhaust gas temperature downstream of the oxidation catalyst, determining the difference between the inlet and the outlet temperatures ( $\Delta T$ ) and adjusting the rate of reductant addition so that  $\Delta T$  is within a pre-determined range.

25           One problem with the application of the second aspect to systems including a NO<sub>x</sub>-trap is that it may be necessary to use rich (i.e.  $\lambda < 1$ ) exhaust gas to regenerate the NO<sub>x</sub>-trap. We propose three embodiments to enable the second aspect of the present invention to be extended to such NO<sub>x</sub>-traps without the need for secondary  
30       air injection.

In a first embodiment shown in Figure 5, at least two NO<sub>x</sub>-traps are arranged in parallel, each with an associated reductant injector. The gas hourly space velocity (GHSV) over each NO<sub>x</sub>-trap is dependent on the relative backpressure in each line, but normally the system will be set up so that the arrangement is the same in each, in which case the GHSV will be substantially the same in each line. NO<sub>x</sub>-trap regeneration is conducted in series in the NO<sub>x</sub>-traps in the system, i.e. at any instant, at least one line is not having reductant injected, so that when the exhaust gas from all NO<sub>x</sub>-traps in the system is mixed, its composition is lean, i.e.  $\lambda > 1$ . The mixed exhaust gas is passed to the oxidation catalyst of the second aspect invention described hereinabove.

In a second embodiment shown in Figure 6A and 6B, a NO<sub>x</sub>-trap is coated on a single substrate monolith and at least two injectors are disposed on the upstream side of the substrate monolith and the arrangement is such that injected reductant is directed to a specific zone of the monolith substrate.

An advantage of this embodiment is that less space is required on the vehicle to accommodate the system compared with the first embodiment and other systems using parallel NO<sub>x</sub>-traps.

A third embodiment is similar to the second embodiment and is shown in Figures 7 and 8. It comprises an upstream three-way flap valve and a reductant injector located either side of the flap valve. During NO<sub>x</sub>-trap "filling" the flap valve can be trimmed so that it lies parallel to the direction of exhaust gas flow. During regeneration, the flap valve is deployed to fold over on the side of the NO<sub>x</sub>-trap receiving the reductant, thereby directing a portion of the exhaust gas flow away from the NO<sub>x</sub>-trap being regenerated and reducing the flow of exhaust gas therein.

An advantage of this embodiment is that the reduced exhaust gas flow in the portion of the NO<sub>x</sub>-trap to be regenerated promotes reduction of the released NO<sub>x</sub> so that regeneration can be done more efficiently than in the second embodiment, i.e. less reductant is required. Furthermore, we believe that the second and third embodiments are patentably novel and inventive in their own right.

Therefore, according to a third aspect, the invention provides an exhaust system for a vehicular lean-burn internal combustion engine comprising a NO<sub>x</sub>-trap disposed on a unitary monolith substrate, the upstream end of which substrate is subdivided in the direction of fluid flow into at least two zones and means for successively contacting a  
5 fraction of the at least two zones with a reductant whilst the NO<sub>x</sub>-trap as a whole remains in-line to exhaust gas flow.

In one embodiment, the means for contacting the NO<sub>x</sub>-trap with reductant comprises an injector disposed sufficiently close to the upstream end of the substrate so  
10 that liquid droplets of reductant contact the NO<sub>x</sub>-trap. The intention of injecting reductant into the exhaust gas upstream of a NO<sub>x</sub>-trap is to reduce the oxygen concentration of the exhaust gas, i.e. to enrich, but not necessarily to make rich ( $\lambda < 1$ ), the exhaust gas composition. In prior art arrangements, reductant is introduced far upstream of the NO<sub>x</sub>-trap, e.g. during the exhaust stroke of one or more engine cylinders  
15 or, in the case of EP 0758713A (incorporated herein by reference), for example, reductant is injected into the exhaust conduit upstream of an oxidation catalyst and diesel particulate filter disposed upstream of the NO<sub>x</sub>-trap. In either case, the droplets of liquid reductant evaporate. Furthermore, at full gas flow, a significant amount of reductant is required merely to remove all the excess oxygen (through combustion) before any degree  
20 of richness is obtained. Where the reductant is a hydrocarbon fuel such as Diesel, this approach is costly on fuel economy.

We have found that by deliberately restricting evaporation of injected fuel by introducing controlled size fuel droplets close to the upstream face of the NO<sub>x</sub>-trap  
25 catalyst, liquid droplets of fuel can impinge on the catalyst surface. Where they do, the environment is strongly reducing and this can reduce stored nitrate in the vicinity. Hence, this arrangement can significantly reduce the fuel penalty associated with NO<sub>x</sub>-trap regeneration.

30 Particle dynamics can cause the droplets of liquid reductant to pass through a conventional flow-through ceramic or metal monolith substrate without impinging on the NO<sub>x</sub>-absorbent carried on the walls thereof. In order to increase the possibility of the reductant contacting the NO<sub>x</sub>-absorbent, in one embodiment a foam substrate comprising

a ceramic or metal foam is used. An alternative embodiment utilises metallic partial filter substrates including internal baffles, such as disclosed in EP-A-1057519 or WO 03/038248 (both incorporated herein by reference). According to a further embodiment, the NO<sub>x</sub>-trap comprises a conventional ceramic wall-flow filter; here pressure-drop  
5 driven convention should ensure that fuel droplets contact stored NO<sub>x</sub>. In this latter embodiment, efficient filtration of particulate matter (PM) *per se* is not important so porous filters could be used, but combined NO<sub>x</sub> and PM control would be desirable as described in JP-B-2722987 (JP-A-06-159037) (incorporated herein by reference), i.e. the filter includes a soot combustion catalyst/NO oxidation catalyst e.g. Pt, a NO<sub>x</sub> absorber  
10 such as barium oxide and, optionally, a NO<sub>x</sub> reduction catalyst e.g. rhodium.

Advantage can also be made of particle dynamics when an oxidation catalyst is coated on a conventional flow-through monolith disposed between the reductant injector and the NO<sub>x</sub>-trap. Depending on the open-frontal area and cell density of the monolith,  
15 fuel droplets can pass through the oxidation catalyst substantially without oxidation and be available for reducing stored NO<sub>x</sub> in the NO<sub>x</sub>-trap. By contrast, evaporated hydrocarbon reductant is more likely to be oxidised on the oxidation catalyst.

According to a further embodiment, the means for contacting the NO<sub>x</sub>-trap  
20 fraction with reductant comprises a flap valve disposed on the upstream end of the substrate thereby to subdivide the substrate into the at least two zones. In one arrangement, an injector is associated with each zone.

In a method of the third aspect, a NO<sub>x</sub>-trap disposed on a monolith substrate in  
25 the exhaust system of a vehicular lean-burn internal combustion engine is regenerated by contacting a fraction of the NO<sub>x</sub>-trap with a reductant while the NO<sub>x</sub>-trap as a whole remains in-line to exhaust gas flow.

In one embodiment, the reductant contacts the fraction of the NO<sub>x</sub>-trap at reduced  
30 exhaust gas flow.

According to a fourth aspect of the invention, there is provided an exhaust system for a vehicular lean-burn internal combustion engine comprising a NO<sub>x</sub> reduction

A method of reducing NO<sub>x</sub> in the exhaust gas of a vehicular internal combustion engine according to the fourth aspect comprises introducing a reductant into the exhaust gas, at all vehicle speeds in a duty cycle, at a rate correlating with a desired NO<sub>x</sub> conversion at the average duty cycle speed and contacting the exhaust gas containing the NO<sub>x</sub> and the reductant with a NO<sub>x</sub> reduction catalyst.

In a particular arrangement, the NO<sub>x</sub> reduction catalysts and systems for delivering reductant described herein are disposed downstream of the arrangement described in EP-B-0341832, mentioned hereinabove.

Unless otherwise described, the catalysts for use in the present invention are coated on high surface area substrate monoliths made from metal or ceramic or silicon carbide, e.g. cordierite, materials. A common arrangement is a honeycomb, flowthrough monolith structure of from 100-600 cells per square inch (cpsi) such as 300-400 cpsi (15.5-93.0 cells cm<sup>-2</sup>, e.g. 46.5-62.0 cells cm<sup>-2</sup>).

The internal combustion engine can be a diesel or lean-burn gasoline engine, such as a gasoline direct injection engine. The diesel engine can be a light-duty engine or a heavy-duty engine, as defined by the relevant legislation.

In order that the present invention may be more fully understood, embodiments thereof will be described with reference to the accompanying drawings, in which:

Figure 1 is a schematic of a system according to the first aspect of the invention;

Figure 2A is a schematic graph plotting NO<sub>x</sub> concentration in the exhaust gas of the system of Figure 1 against engine load;

Figure 2B is a schematic graph plotting temperature in the exhaust gas of the system of Figure 1 against engine load;

catalyst, a reductant injector disposed upstream of the catalyst and means, when in use, for controlling reductant addition, wherein the reductant addition control means supplies reductant to the catalyst at a rate which is predetermined to correlate with a desired NO<sub>x</sub> conversion at the average duty cycle speed of the vehicle at all vehicle speeds in a duty cycle.

The invention of the fourth aspect has particular application to the retrofit market for vehicles of a limited duty cycle such as buses or refuse trucks. The idea is to determine what rate of reductant injection is required to reduce a chosen quantity of NO<sub>x</sub>, e.g. 90%, in a NO<sub>x</sub> reduction catalyst at the average duty cycle speed. For example, when the NO<sub>x</sub> reduction catalyst comprises a NO<sub>x</sub>-trap, the system controller can be arranged, when in use, to generate a continuous tempo and quantity of HC fuel injection e.g. injection at 2 seconds every minute. The system controller can also be arranged to provide occasional relatively long rich HC fuel pulses to ensure that the NO<sub>x</sub>-trap is substantially completely regenerated, followed by the more frequent sequence of shorter enrichment pulses to maintain the storing capability of the NO<sub>x</sub>-trap. The exact detail of the injection strategy depends on the vehicle and its duty cycle.

At speeds higher than the average duty cycle speed, there would be more NO<sub>x</sub> and a greater mass airflow and so NO<sub>x</sub> conversion overall would fall off, because of insufficient reductant but because higher speed would be less likely e.g. in city centre buses, the increased fuel penalty for NO<sub>x</sub> conversion achieved resulting from such higher speeds would be less across the entire drive cycle compared with prior art arrangements, e.g. that use delayed injection timing. The correlation of the rate of HC injection to average duty cycle speed can be tailored to the particular application, e.g. buses in Manchester (UK) city centre would be expected to encounter different duty cycles to those in London (UK).

In one embodiment of the fourth aspect, an oxidation catalyst is disposed between the reductant injector and the NO<sub>x</sub>-trap for increasing the temperature of the NO<sub>x</sub>-trap for regeneration and to remove oxygen from the exhaust gas to ensure a rich exhaust gas for regeneration of the NO<sub>x</sub>-trap.

Figure 2C is a schematic graph plotting temperature in the exhaust gas of the system of Figure 1 against  $\text{NO}_x$  concentration (left hand y-axis) and reductant addition (right-hand y-axis);

5        Figure 3 is a schematic of a system according to the second aspect of the invention;

Figure 4A is a schematic graph plotting  $\text{NO}_x$  reduced over the  $\text{NO}_x$  reduction catalyst in the system of Figure 3 against reductant addition;

10

Figure 4B is a schematic graph plotting  $\text{NO}_x$  reduced over the  $\text{NO}_x$  reduction catalyst in the system of Figure 3 against  $\Delta T$  showing addition of reductant at above a critical temperature (hashed line to x-axis) and optimal reductant addition corresponding to detected  $\Delta T$  (shaded region);

15

Figure 5 is a schematic of a system according to one embodiment of the second aspect of the invention;

20        Figure 6A is a schematic of another embodiment of the second aspect of the invention showing an end-on view of a  $\text{NO}_x$ -trap comprising a unitary substrate monolith showing the injection points and spray zones of multiple reductant injectors at the upstream end of the substrate;

25        Figure 6B is a schematic side view of the unitary substrate monolith shown in Figure 6A;

Figure 7 is a schematic sectional view of an embodiment of the third aspect of the invention including a  $\text{NO}_x$ -trap in combination with a soot combustion reactor for use in treating the exhaust gas of a diesel engine;

30

Figure 8 shows another embodiment of the third aspect of the invention comprising a  $\text{NO}_x$ -trap similar to that of Figure 7 but using a two-part soot combustion reactor, the second part housing a flow-reversing filter;

Figures 9A (position 123A) and 9B (position 123B) show enlarged plan views of a 4-way valve as used in Figure 8 representing the two extreme positions of the valve;

5 Figure 10 shows a schematic system according to the fourth aspect of the invention; and

Figure 11 is a schematic graph plotting quantity of fuel against time showing a fuel injection strategy for use in the system of Figure 9.

10 A system according to the first aspect of the invention generally referenced by the numeral 10 is depicted in Figure 1 in which 12 represents a diesel engine, 14 the exhaust manifold, 16 the exhaust line and 18 a NO<sub>x</sub> reduction catalyst, such as a 5wt%Cu/Beta-zeolite lean-NO<sub>x</sub> catalyst. Reductant supply means 20 includes an injector for injecting a  
15 quantity of diesel fuel into the exhaust line 16 upstream of catalyst 18. Thermocouple TC1 detects the temperature of the exhaust gas at the inlet to catalyst 18 and relays the detected temperature to a processor in the engine control unit (ECU (not shown)).

20 As the load on an engine is increased, the NO<sub>x</sub> level in the exhaust gas increases in an approximately linear manner. Similarly, the exhaust gas temperature increases with load. Below a certain critical temperature no reductant is added because the temperature is too low for the complete NO<sub>x</sub> removal reaction to take place. Figures 2A and 2B show in graphical form representations of correlations of exhaust gas NO<sub>x</sub> concentration against engine load and temperature against engine load over a duty cycle  
25 of particular engine 12. In practice, the actual amount of reductant added at different exhaust gas temperatures will depend on the nature of the specific duty cycle, but there will be a trend for more reductant to be needed to remove larger amounts of NO<sub>x</sub> at higher temperatures. Such determinations can be conducted using appropriate apparatus and techniques known to the person skilled in the art e.g. using a suitable engine  
30 dynamometer and NO<sub>x</sub> sensor. From these measurements it is possible to calculate the rate of reductant addition required to reduce the NO<sub>x</sub> in the exhaust gas to N<sub>2</sub> on the catalyst over the drive cycle and to correlate this with exhaust gas temperature, as shown in Figure 2C. The correlations can be loaded onto the ECU processor of a fleet of such



vehicles operating the system of Figure 1 and stored as look up tables. In use, the rate and quantity of reductant addition is controlled by the ECU to be proportional to the temperature of the exhaust gas as detected by thermocouple TC1. Addition of reductant in this way provides an efficient and simple way of controlling NO<sub>x</sub> reduction on a  
5 vehicle.

A system, generally referenced as 30, according to one embodiment according to the second aspect of the invention is shown in Figure 3, with like features from Figure 1 sharing the same reference numerals. The additional features new to the system of  
10 Figure 1 shown in Figure 3 include oxidation catalyst 32, e.g. 1wt% platinum supported on a gamma-alumina washcoat, that TC1 is located downstream of NO<sub>x</sub> reduction catalyst 18 between catalyst 18 and oxidation catalyst 32 and a second thermocouple TC2 is located downstream of oxidation catalyst 32.

15 In use, the system is operated in such a way as to ensure the gas is always lean over the oxidation catalyst 32. As in the system of Figure 1, no reductant is added below a certain critical exhaust gas temperature, at which the NO<sub>x</sub> reduction catalyst is below its light-off temperature for catalysing NO<sub>x</sub> reduction. Above this temperature, increasing the amount of reductant causes increasing amounts of NO<sub>x</sub> in the exhaust gas  
20 to be reduced. Small excess reductant slip is oxidised over oxidation catalyst 32 and the resulting exotherm results in a temperature increase across the catalyst as measured by the difference in temperatures detected at TC2 and TC1, i.e.  $\Delta T = TC2 - TC1$ . The control strategy is to adjust the rate of reductant addition to keep the measured  $\Delta T$  at substantially a pre-determined value corresponding to optimum NO<sub>x</sub> removal.  
25 The reductant flow is increased if  $\Delta T$  is too small, or decreased if  $\Delta T$  is larger than desired for optimum efficient NO<sub>x</sub> conversion.

A system, generally referenced as 40, according to a second embodiment of the second aspect of the invention is shown in Figure 5, with like features from Figure 3  
30 sharing the same reference numerals. The additional features new to the system of Figure 3 shown in Figure 5 include multiple NO<sub>x</sub>-traps 42 arranged in parallel exhaust lines 44, each line having its own reductant supply means 20.

This arrangement of the second aspect according to the invention and shown in Figure 3 presents no particular problem when applied to lean NO<sub>x</sub> catalyst or ammonia SCR systems that operate under lean conditions, but NO<sub>x</sub>-trap 42 regeneration is more problematical. One problem resulting from the need for rich NO<sub>x</sub>-trap regeneration is that downstream oxidation catalyst 32 cannot remove excess reductant in a deficiency of oxygen. This could lead to high tailpipe reductant emissions as well as other possible problems.

The system of Figure 5 shows how it is possible to split the exhaust gas flow into two or more parallel lines 44 each with its own NO<sub>x</sub>-trap 42 and reductant injector 20. At any one time, at least one line is not having reductant injected, so when the total NO<sub>x</sub>-trap 42 exit gas streams are mixed, the resulting gas is overall lean before passing over the downstream oxidation catalyst 32. In this way any excess reductant is oxidised, and the resulting  $\Delta T$  can be used to control the NO<sub>x</sub>-reduction system as described for the Figure 3 embodiment above.

A third embodiment of the second aspect of the invention is shown in Figures 6A and 6B, wherein the plurality of parallel NO<sub>x</sub>-traps 42 of the Figure 5 embodiment are replaced by a single unitary NO<sub>x</sub>-trap 42A and three reductant supply means 20 disposed equidistantly at the upstream end of the NO<sub>x</sub>-trap and directing a reductant spray onto juxtaposed zones 45 on the front face of the substrate monolith whose centres are defined by injection points 46. This arrangement provides the same overall effect as the first embodiment illustrated in Figure 5 but using a larger single, i.e. unitary NO<sub>x</sub>-trap equipped with two or more reductant injectors. The injectors are operated in a sequential manner so at any one time only part of the NO<sub>x</sub>-trap is undergoing regeneration, and exit gas from this part is mixed with exhaust gas from parts not being regenerated to provide an overall lean gas stream for oxidation on catalyst 32.

The reductant supply means for this embodiment can be arranged to provide a controlled size of fuel droplets close to the catalyst front so that liquid droplets impinge on the catalyst surface. Where they do, the environment will be strongly reducing and reduce stored nitrate in the vicinity. An advantage of this arrangement is that the fuel

penalty for NO<sub>x</sub>-trap regeneration is less than for a system employing modulation of injection timing in one or more cylinders of the engine.

Referring to Figure 7, an exhaust gas aftertreatment system 80 comprises a soot combustion reactor 120 the inlet of which is connected to the exhaust manifold of a diesel engine (not shown). Reactor 120 at its upstream portion contains oxidation catalyst 122 consisting of a ceramic honeycomb carrying an alumina-based washcoat and Pt. At its downstream portion reactor 120 contains wall-flow filter 124, consisting of filter-grade ceramic honeycomb, the passages of which are alternately plugged and unplugged at the inlet end and alternately plugged at the outlet end, wherein passages plugged at the inlet end are unplugged at the outlet end, and *vice versa*. Such an arrangement is described in EP-B-0341832 and the arrangement is known as the CRT<sup>®</sup>. From the outlet end of reactor 120 plenum 126 continues as the operating chamber of flap valve 128X,Y,Z at the inlet of NO<sub>x</sub>-trap vessel 130. Vessel 130 contains NO<sub>x</sub>-trap 131X,Y consisting of a flowthrough ceramic honeycomb monolith substrate carrying an alumina washcoat containing barium oxide and metallic Pt and Rh. The fulcrum of flap valve 128X,Y,Z is mounted on partition 129 which extends diametrically across the face of reactor 130 and is gas-tightly sealed to the face of NO<sub>x</sub>-trap 131. Each region X,Y of reactor 130 either side of valve 128 is provided with reactant injector 132X,Y. In the complete reactor 130 as shown, valve 128 is in the central position Z. Valve positions X and Y are shown as insets. Reactor 130 is formed with outlet 134, leading to atmosphere or to further treatment. Preferably, rates of flow in the two halves of reactor 130 are controlled to give a net lean composition and the mixture is passed over an oxidat, in the arrangement shown in Figure 3 or 5.

25

In the normal operation of the system, the exhaust gas, comprising steam (H<sub>2</sub>O (g)), dinitrogen (N<sub>2</sub>), oxygen (O<sub>2</sub>), carbon dioxide (CO<sub>2</sub>), unburned hydrocarbon fuel (HC), carbon monoxide (CO), nitrogen oxides (NO<sub>x</sub>) and particulate matter (PM), at e.g. 300°C contacts catalyst 122 over which NO is oxidised to NO<sub>2</sub> and some of the HC and CO are oxidised to steam and CO<sub>2</sub>. It then enters filter 124 on which most of the PM is collected and combusted by reaction with the NO<sub>2</sub> formed in catalyst 122 and possibly with O<sub>2</sub>. The PM-freed gas then undergoes treatment in one of the 3 modes: 128Z: NO<sub>x</sub>-trap regions 130X and 130Y both absorb (or adsorb) NO<sub>x</sub>; 128X:

30

region 131X receives a small fraction of the gas leaving plenum 126 and injection of diesel fuel at 132X. It undergoes regeneration, and its effluent is reunited with that of region 130Y; region 131Y receives the major portion of the gas, absorbs NO<sub>x</sub> and passes its effluent to atmosphere at 134; 128Y: region 131Y performs the duty  
5 described at 128X.

The engine management system (not shown) changes from region X to region Y when NO<sub>x</sub>-trap 131Y has free capacity to absorb NO<sub>x</sub>; and *vice versa*.

10 Referring to Figure 8, an alternative exhaust system to the one shown in Figure 7 is referenced generally by numeral 90 with common features from Figure 7 having the same reference numbers, wherein reactor 120 now only contains catalyst 122. The PM filter vessel, now numbered 125, is in separate vessel 121. It differs in providing for reversal of the direction of flow through the filter. The outlet of reactor 120 is connected  
15 to filter vessel 121 by way of 4-way valve 123, operable in positions 123A and 123B (inset), to give respectively right-hand to left-hand and left-hand to right-hand flow through filter 125, but with no blocking mid-point; since the midpoint bypasses filter 125. Operation of valve 123 is controlled to be very rapid. Leaving filter 125 in either direction, the gas passes through valve 123A or B to NO<sub>x</sub>-trap 130, which is structurally  
20 and functionally as in Figure 7.

A characteristic of modern diesel engines is that engine out NO<sub>x</sub> and/or exhaust gas temperature can be too low for passive filter regeneration using NO<sub>2</sub> generated catalytically by oxidation of NO as described in EP-B-0341832. One solution to this  
25 problem is to regenerate the filter actively by increasing the temperature in the exhaust system thereby to combust PM on the filter and maintain the back pressure across the filter within acceptable design tolerances. Such active regeneration techniques are described in EP 0758713A, for example.

30 An advantage of the system disclosed in Figure 8 to the practical application of the CRT<sup>®</sup> process is that flow reversal in the filter can be used to clear PM that is not readily combusted in NO<sub>2</sub> over a drive cycle. The uncombusted PM can be collected on a second, disposable filter for removal at suitable intervals. Thus, the arrangement has

particular use to the retrofit market, providing a practical and economic alternative to installing expensive and fuel-costly active regeneration apparatus.

To switch the direction of gas flow in the embodiment shown in Figure 8, a suitable 4-way valve 123 can be used and is shown in Figures 9A and 9B. The plan views shown in these figures relate to an essentially cylindrical valve casing 100 formed internally with circumferential regions 102 of greater diameter, defining the range of traverse of rectangular butterfly deflector 104 having pivoted operating shaft 106 extending out of the valve casing via a seal to an actuator (not shown). The extremities of the range of traverse are defined by steps 108 between the regions differing in diameter, such steps limiting gas leakage out of its intended path. 'LHS' stands for 'left-hand side' and RHS for 'right hand side'.

The arrangements shown in Figure 7, 8 and 9 are considered independently inventive for at least the reasons given below. In-system valving is known to be desirable to avoid complicated piping, but its adoption has been limited because valve mechanisms suffer corrosion in relatively hot exhaust gas resulting in pre-end-of-life valve replacement. This concern is particularly relevant in heavy-duty diesel vehicles.. However, in the present arrangement, the gas is diesel exhaust which, especially in modern engines, is not as hot as prior art engines; the exhaust gas is relatively low in  $\text{SO}_x$  because low sulfur diesel is used; downstream of the filter, the gas contains relatively little PM which could foul the valve; and the gas is lean, therefore passivating to steel. Hence, the combination of the features makes in-system valving a practical proposition.

In the system 50 depicted in Figure 10, 52 is a conditional system controller (CSC), 54 is a master switch, 56 is an alternator, 58 is a blocking capacitor, 60 is a thermocouple, 62 is an injection controller (ICU), 64 is a fuel pump, 66 is a valve, 68 is a fuel injector and 70 is a positive power line. The CSC 52 is a switch providing power to the ICU 62 if the master power switch 54 is on, the engine is running as determined by an AC ripple from the alternator 56 present after a DC blocking capacitor 58 and the output of a suitably placed thermocouple 60 to detect the exhaust system is above a minimum pre-determined temperature for reduction of  $\text{NO}_x$  on a suitable  $\text{NO}_x$ -trap. The master switch 54 need not be connected to the key-on position.

The CSC 52 is designed to generate a continuous tempo and quantity of HC injection when all three features (master switch position, detection of alternator ripple and exhaust gas temperature above a pre-determined minimum) coincide. When the  
5 CSC 52 is on, power is supplied to the injection pump 64 and the ICU 62 that operates a solenoid valve 66 to produce a series of pulses to enrich the exhaust gas before it passes over an oxidation catalyst upstream of the NO<sub>x</sub> absorbing components. Typically the injection controller will provide occasional relatively very long rich pulses to ensure that the NO<sub>x</sub>-trap is substantially completely empty and this is followed by a more frequent  
10 sequence of shorter enrichment pulses, e.g. injection at 2 seconds every minute, to maintain the storing capability of the NO<sub>x</sub>-trap (see Figure 11).

This fuel injection rate is correlated to a chosen NO<sub>x</sub> conversion e.g. 90% at the average duty cycle speed. At higher speeds than the average duty cycle speed, there is  
15 more NO<sub>x</sub> and a greater mass airflow and so NO<sub>x</sub> conversion would fall off. However, because higher speeds are less likely, e.g. in city centre buses or refuse trucks, the increased fuel penalty for NO<sub>x</sub> conversion achieved resulting from such higher speeds is less across the entire drive cycle compared with prior art arrangements, e.g. that use delayed injection timing. The exact detail of the injection strategy depends on the  
20 vehicle and its duty cycle.

Whilst, very generally, the systems employing NO<sub>x</sub>-traps described herein have been developed to provide simple control mechanisms to predict when NO<sub>x</sub>-trap regeneration should be done, with particular application to retrofit, many vehicles  
25 already include a range of sensors to input data to the ECU for controlling other aspects of vehicular operation. By suitable re-programming of the ECU it is possible to adopt one or more of such existing sensor inputs for the purposes of predicting remaining NO<sub>x</sub>-trap capacity. These include, but are not limited to, predetermined or predicted time elapsed from key-on or previous regeneration, by sensing the status of a suitable clock means; airflow over the TWC or manifold vacuum; ignition timing; engine speed;  
30 throttle position; exhaust gas redox composition, for example using a lambda sensor, preferably a linear lambda sensor; quantity of fuel injected in the engine; where the vehicle includes an exhaust gas recirculation (EGR) circuit, the position of the EGR valve and thereby the detected amount of EGR; engine coolant temperature; and where

the exhaust system includes a NO<sub>x</sub> sensor, the amount of NO<sub>x</sub> detected upstream and/or downstream of the NO<sub>x</sub>-trap. Where the clock embodiment is used, the predicted time can be subsequently adjusted in response to data input.

**CLAIMS:**

- 5 1. An exhaust system (10) for a vehicular lean-burn internal combustion engine (12), which system comprising a catalyst (18) for reducing  $\text{NO}_x$  in exhaust gas to  $\text{N}_2$  with a suitable reductant, a source of reductant, means (20) for contacting the catalyst (18) with the reductant, means (TC1) for sensing the temperature of the exhaust gas and/or the catalyst bed and means, when in use, for controlling reductant addition, wherein the
- 10 reductant addition control means supplies an amount of reductant to the catalyst at a rate corresponding to a measured temperature value of the exhaust gas and/or catalyst bed, which temperature value has been pre-determined to correlate, in use, with an amount of  $\text{NO}_x$  in the exhaust gas thereby to promote the reduction of the  $\text{NO}_x$ .
- 15 2. A method of calibrating a rate of reductant addition required to reduce  $\text{NO}_x$  in an exhaust gas of a vehicular lean-burn internal combustion engine (12) to  $\text{N}_2$  over a suitable catalyst (18), which method comprising measuring  $\text{NO}_x$  in the exhaust gas at a plurality of exhaust gas and/or catalyst bed temperatures and correlating each exhaust gas and/or catalyst bed temperature value with a rate of reductant addition required to
- 20 reduce the  $\text{NO}_x$  over the catalyst.
3. An exhaust system (30; 40) for a vehicular lean-burn internal combustion engine (12), which system comprising a catalyst (18; 42; 42A) for reducing  $\text{NO}_x$  in exhaust gas to  $\text{N}_2$  with a suitable reductant, a source of reductant, means (20) for contacting the  $\text{NO}_x$
- 25 reduction catalyst (18; 42; 42A) with the reductant, an oxidation catalyst (32) disposed downstream of the  $\text{NO}_x$  reduction catalyst (18; 42; 42A), means (TC1, TC2) for determining a temperature difference ( $\Delta T$ ) across the oxidation catalyst (32) and means, when in use, for controlling reductant addition, wherein the reductant addition control means controls the rate of reductant addition to maintain  $\Delta T$  within a pre-determined
- 30 range, wherein the system is configured so that the exhaust gas composition over the oxidation catalyst is lean.
4. A method of controlling, by feedback, addition of reductant to a catalyst (18; 42; 42A) for reducing  $\text{NO}_x$  in an exhaust gas of a vehicular lean-burn internal combustion



engine (12) to N<sub>2</sub>, which method comprising providing an oxidation catalyst (32) for oxidising the reductant downstream of the NO<sub>x</sub> reduction catalyst (18; 42; 42A), measuring the exhaust gas temperature upstream of the oxidation catalyst (32), measuring the exhaust gas temperature downstream of the oxidation catalyst (32),  
5 determining the difference between the inlet and the outlet temperatures ( $\Delta T$ ) and adjusting the rate of reductant addition so that  $\Delta T$  is within a pre-determined range.

5. An exhaust system for a vehicular lean-burn internal combustion engine comprising a NO<sub>x</sub>-trap (42A; 131) disposed on a unitary monolith substrate, the  
10 upstream end of which substrate is subdivided in the direction of fluid flow into at least two zones (45; 131X,131Y) and means for successively contacting a fraction of the at least two zones (45; 131X,131Y) with a reductant whilst the NO<sub>x</sub>-trap (42A; 131) as a whole remains in-line to exhaust gas flow.

15 6. An exhaust system according to claim 5, wherein the means for contacting the NO<sub>x</sub>-trap fraction with reductant comprises an injector (20; 132X,132Y) disposed sufficiently close to the upstream end of the substrate so that droplets of liquid reductant contact the NO<sub>x</sub>-trap.

20 7. An exhaust system according to claim 6, wherein the substrate comprises a ceramic or metal foam.

8. An exhaust system according to claim 5, wherein the means for contacting the NO<sub>x</sub>-trap fraction with reductant comprises a flap valve (128) disposed at the upstream  
25 end of the substrate thereby to subdivide the substrate into the at least two zones (131X,131Y).

9. An exhaust system according to claim 8, comprising an injector (132X,132Y) associated with each zone.

30 10. A method of regenerating a NO<sub>x</sub>-trap (42A; 131) disposed on a monolith substrate in the exhaust system of a vehicular lean-burn internal combustion engine,

which method comprising contacting a fraction (45; 131X,131Y) of the NO<sub>x</sub>-trap with a reductant while the NO<sub>x</sub>-trap as a whole remains in-line to exhaust gas flow.

11. A method according to claim 10, wherein the fraction of the NO<sub>x</sub>-trap is  
5 contacted with droplets of liquid reductant.

12. A method according to claim 10, wherein the reductant contacts the fraction of the NO<sub>x</sub>-trap at reduced exhaust gas flow.

10 13. An exhaust system for a vehicular lean-burn internal combustion engine comprising a NO<sub>x</sub> reduction catalyst, a reductant injector (68) disposed upstream of the catalyst and means (50), when in use, for controlling reductant addition, wherein the reductant addition control means supplies reductant to the catalyst at a rate which is predetermined to correlate with a desired NO<sub>x</sub> conversion at the average duty cycle speed  
15 of the vehicle at all vehicle speeds in a duty cycle.

14. An exhaust system according to claim 13, comprising an oxidation catalyst disposed between the reductant injector (68) and the NO<sub>x</sub> reduction catalyst.

20 15. A method of reducing NO<sub>x</sub> in the exhaust gas of a vehicular internal combustion engine, which method comprising introducing a reductant into the exhaust gas, at all vehicle speeds in a duty cycle, at a rate correlating with a desired NO<sub>x</sub> conversion at the average duty cycle speed and contacting the exhaust gas containing the NO<sub>x</sub> and the reductant with a NO<sub>x</sub> reduction catalyst.

25 16. A method according to claim 15, comprising contacting the reductant with an oxidation catalyst upstream of the NO<sub>x</sub> reduction catalyst thereby to increase the temperature of the exhaust gas and/or to reduce the oxygen concentration in the exhaust gas.

30 17. An exhaust system according to any of claims 1, 3, 5 to 9, 13 or 14, comprising control means, when in use, to supply reductant to the NO<sub>x</sub> reduction catalyst only when the NO<sub>x</sub> reduction catalyst is active.

18. A method according to any of claims 2, 4, 10 to 12, 15 or 16, wherein reductant is supplied to the NO<sub>x</sub> reduction catalyst only when it is active for catalysing NO<sub>x</sub> reduction.
- 5 19. An exhaust system according to claim 3, wherein the rate of reductant addition is decreased if  $\Delta T$  is too large.
20. A method according to claim 4, wherein the rate of reductant addition is  
10 decreased if  $\Delta T$  is too large.
21. An exhaust system according to claim 1, 3, 5 to 9, 13, 14 or 17, wherein the reductant is a hydrocarbon and the catalyst is a lean-NO<sub>x</sub> catalyst.
- 15 22. An exhaust system according to claim 1, 3, 5 to 9, 13, 14 or 17, wherein the reductant is a NO<sub>x</sub>-specific reactant and the catalyst is a selective catalytic reduction (SCR) catalyst.
23. An exhaust system according to claim 21 or 22, wherein the catalyst comprises a  
20 NO<sub>x</sub>-absorbent.
24. A method according to claim 2, 4, 10 to 12, 15, 16 or 18, wherein the reductant is a hydrocarbon and the catalyst is a lean-NO<sub>x</sub> catalyst.
- 25 25. A method according to claim 2, 4, 10 to 12, 15, 16 or 18, wherein the reductant is a NO<sub>x</sub>-specific reactant and the catalyst is a selective catalytic reduction (SCR) catalyst.
26. A method according to claim 24 or 25, wherein the catalyst comprises a NO<sub>x</sub>-absorbent.

1 / 7

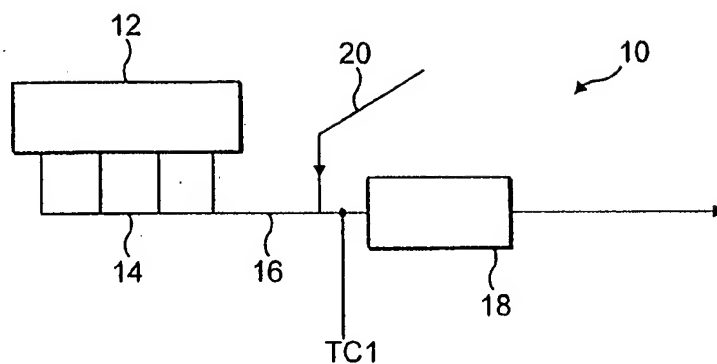


FIG. 1

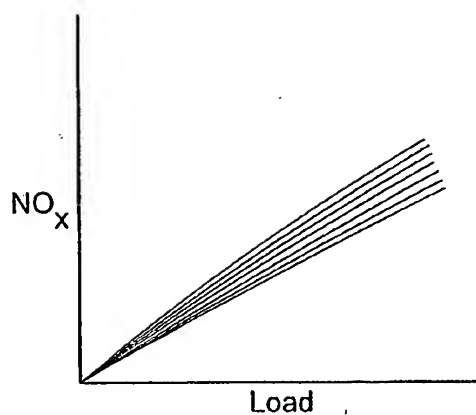


FIG. 2A

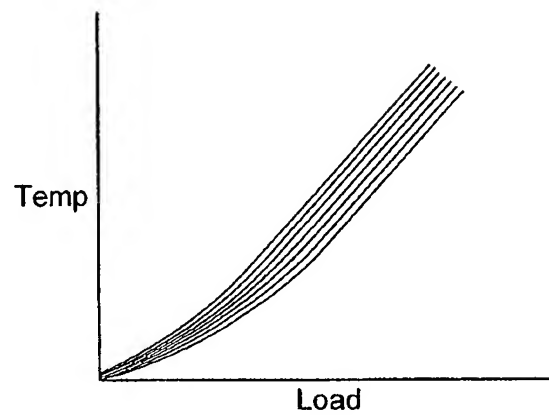


FIG. 2B

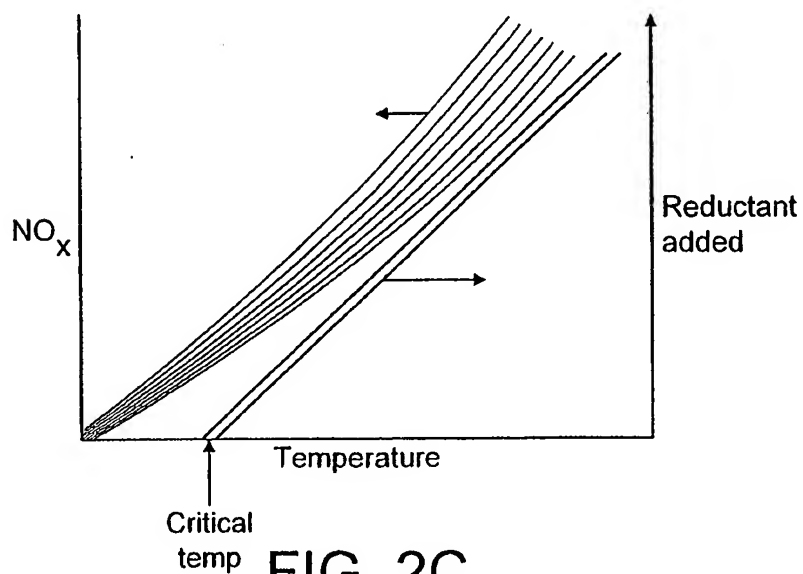


FIG. 2C

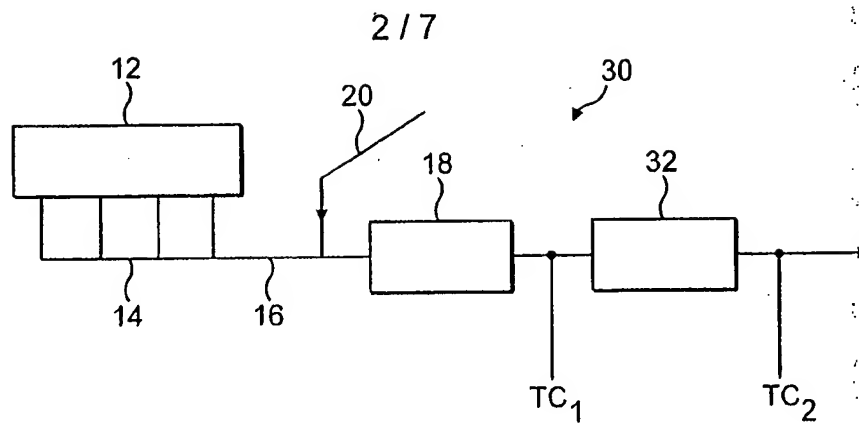


FIG. 3

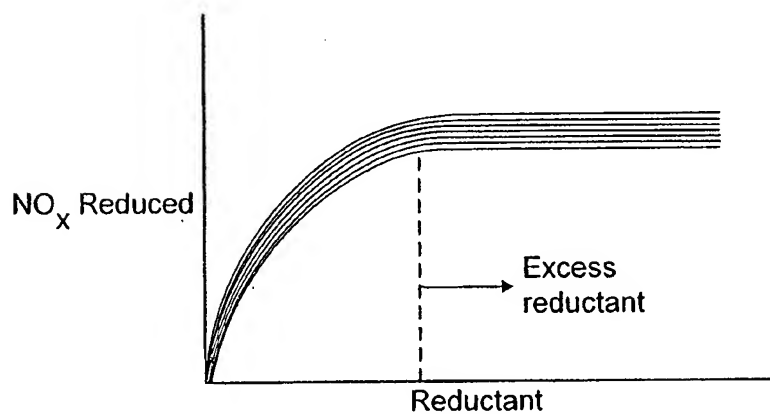


FIG. 4A

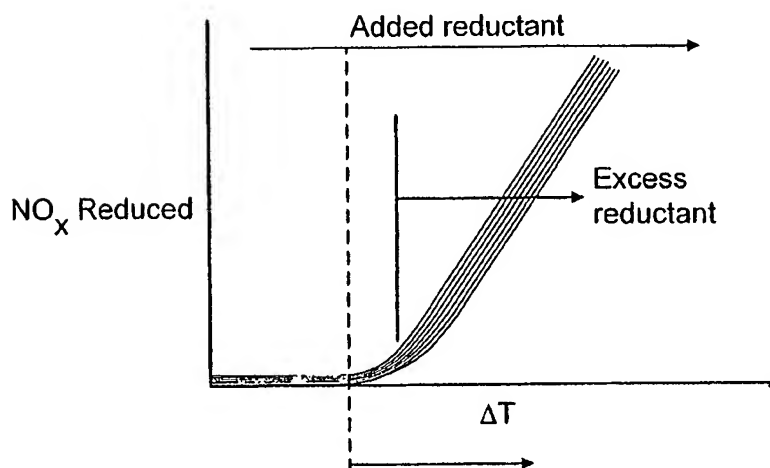
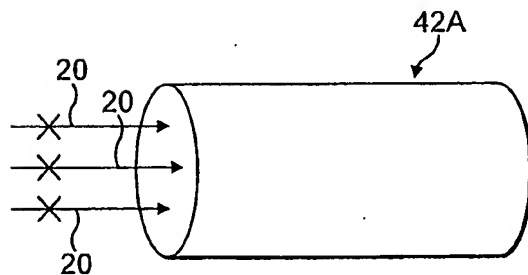
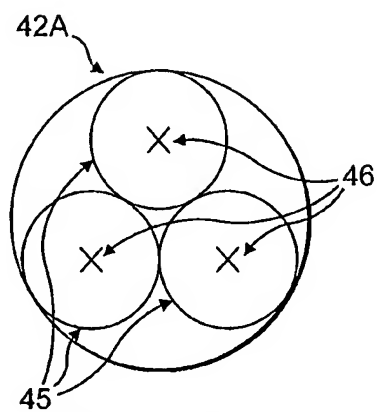
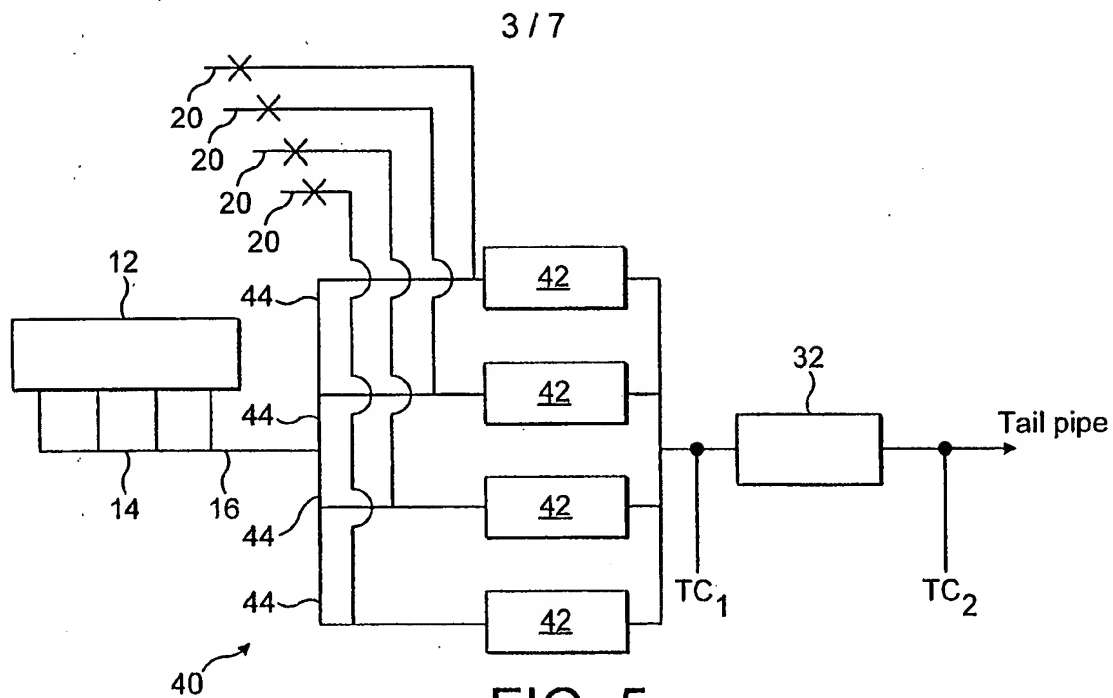


FIG. 4B



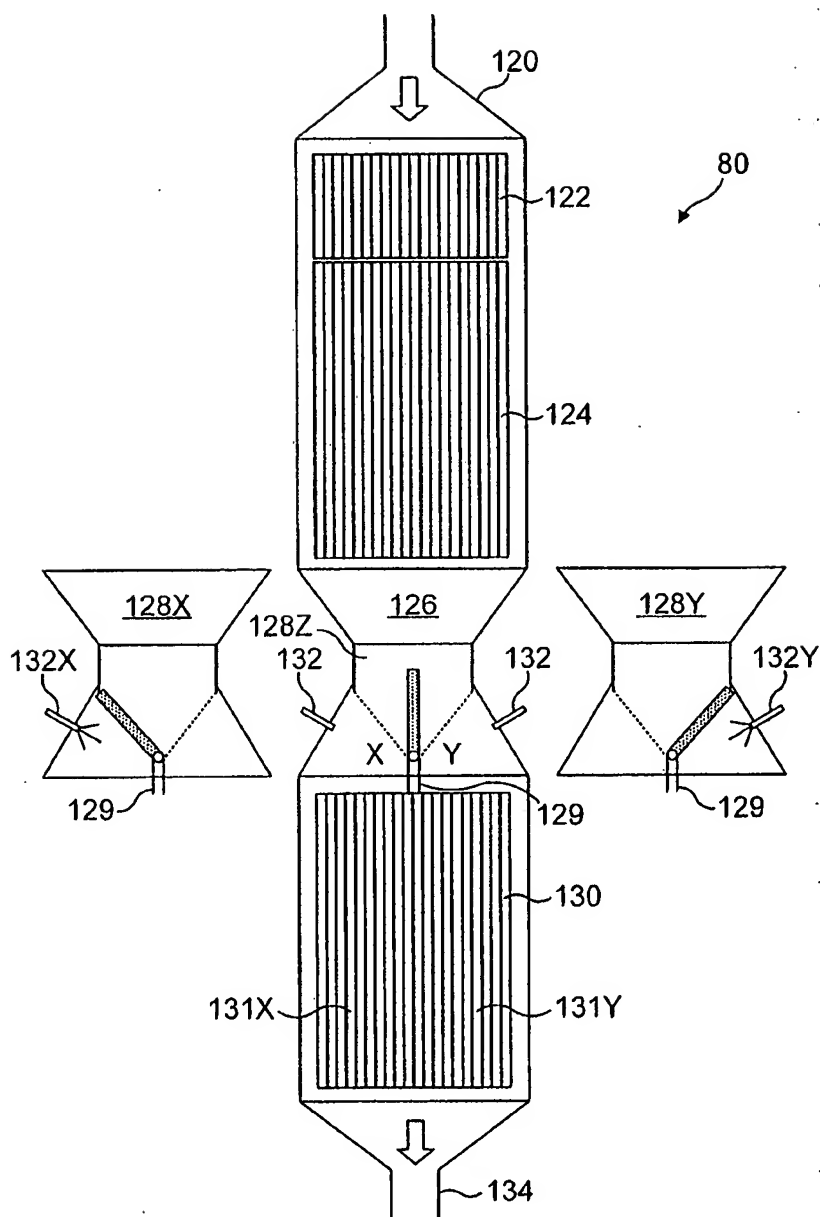


FIG. 7

5 / 7

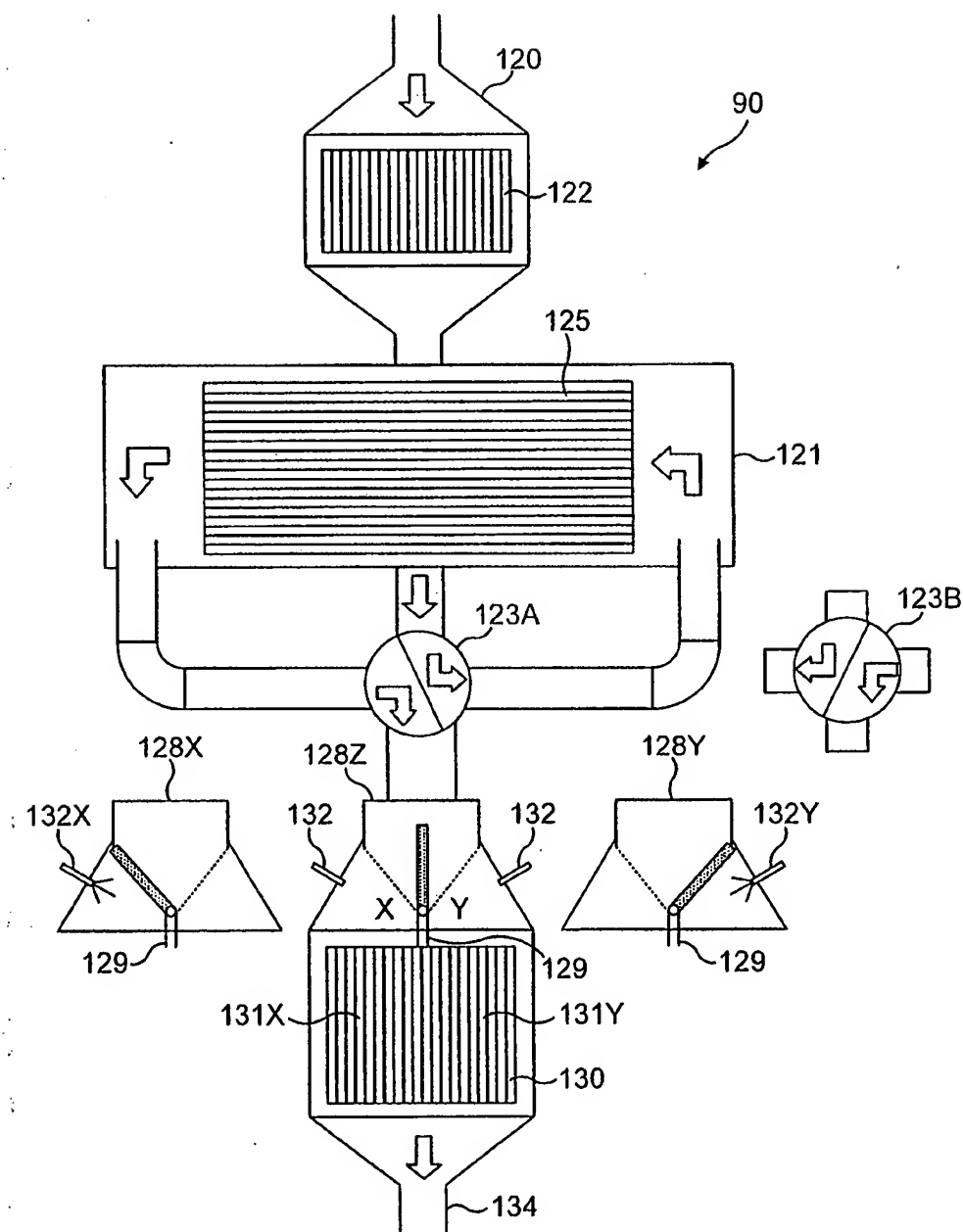


FIG. 8



6 / 7

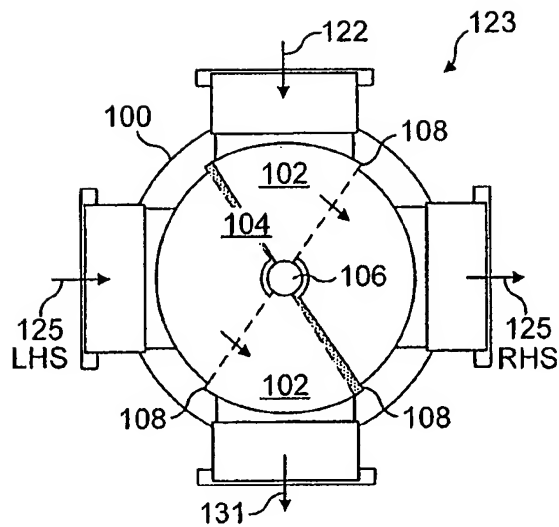


FIG. 9A

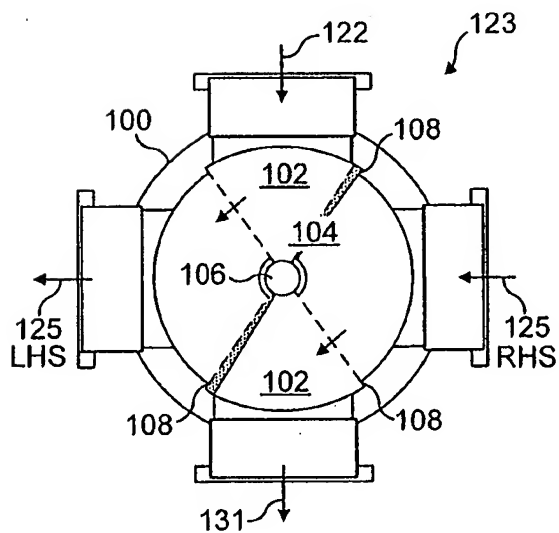


FIG. 9B

7 / 7

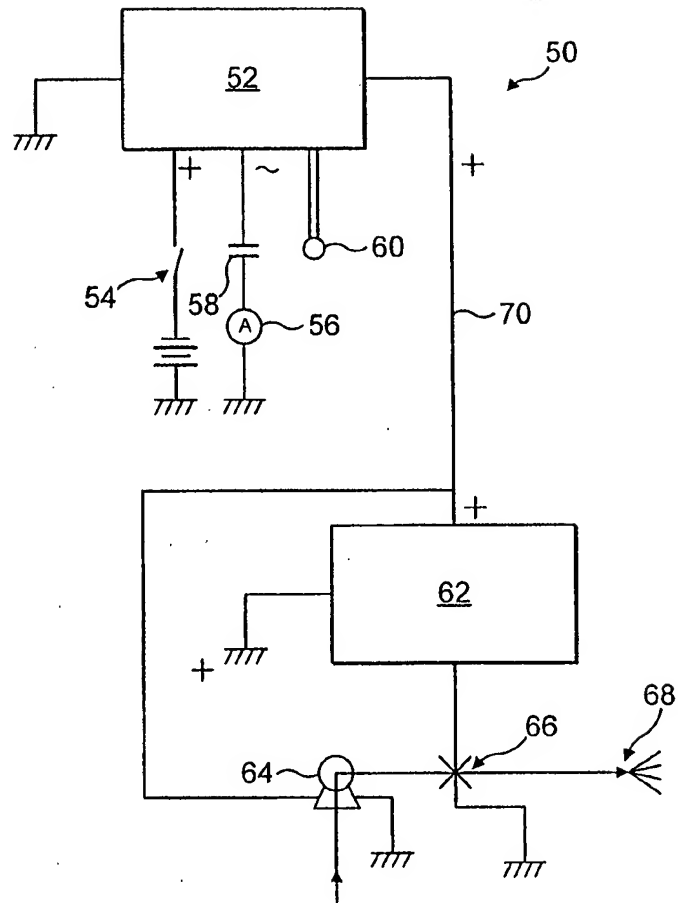


FIG. 10

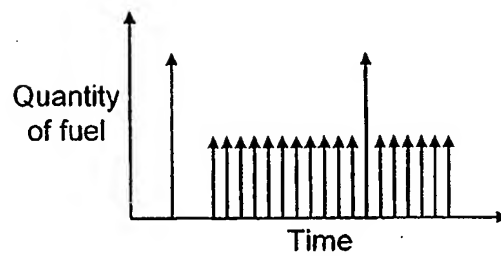


FIG. 11

(19) World Intellectual Property  
Organization  
International Bureau



(43) International Publication Date  
29 December 2004 (29.12.2004)

PCT

(10) International Publication Number  
WO 2004/113691 A3

(51) International Patent Classification: F01N 3/02,  
3/20, 9/00, 11/00

Caxton, Cambridge CB3 8PQ (GB). WALKER, Andrew,  
Peter [GB/GB]; 57 Bramley Avenue, Melbourn, Royston  
SG8 6HG (GB).

(21) International Application Number:  
PCT/GB2004/002643

(74) Agent: NUNN, Andrew, Dominic; Johnson Matthey  
Technology Centre, Blounts Court, Sonning Common,  
Reading RG4 9NH (GB).

(22) International Filing Date: 18 June 2004 (18.06.2004)

(25) Filing Language: English

(26) Publication Language: English

(30) Priority Data:  
0314242.9 18 June 2003 (18.06.2003) GB  
0314463.1 23 June 2003 (23.06.2003) GB  
0322963.0 1 October 2003 (01.10.2003) GB

(81) Designated States (unless otherwise indicated, for every  
kind of national protection available): AE, AG, AL, AM,  
AT, AU, AZ, BA, BB, BG, BR, BW, BY, BZ, CA, CH, CN,  
CO, CR, CU, CZ, DE, DK, DM, DZ, EC, EE, EG, ES, FI,  
GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE,  
KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MA, MD,  
MG, MK, MN, MW, MX, MZ, NA, NI, NO, NZ, OM, PG,  
PH, PL, PT, RO, RU, SC, SD, SE, SG, SK, SL, SY, TJ, TM,  
TN, TR, TT, TZ, UA, UG, US, UZ, VC, VN, YU, ZA, ZM,  
ZW.

(71) Applicant (for all designated States except US): JOHN-  
SON MATTHEY PUBLIC LIMITED COMPANY  
[GB/GB]; 2-4 Cockspur Street, Trafalgar Street, London  
SW1Y 5BQ (GB).

(84) Designated States (unless otherwise indicated, for every  
kind of regional protection available): ARIPO (BW, GH,  
GM, KE, LS, MW, MZ, NA, SD, SI, SZ, TZ, UG, ZM,  
ZW), Eurasian (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM),  
European (AT, BE, BG, CH, CY, CZ, DE, DK, EE, ES, FI,  
FR, GB, GR, HU, IE, IT, LU, MC, NL, PL, PT, RO, SE, SI,  
SK, TR), OAPI (BF, BJ, CF, CG, CI, CM, GA, GN, GQ,  
GW, ML, MR, NE, SN, TD, TG).

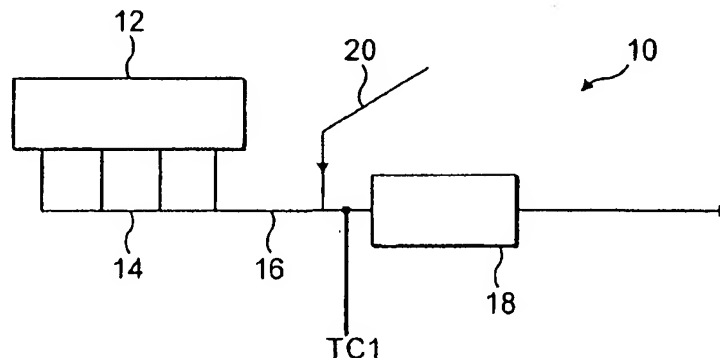
(72) Inventors; and

(75) Inventors/Applicants (for US only): ALLANSSON,  
Elve, Tord, Ronny [SE/SE]; Norra Annebergsvagen 123,  
S-434 96 Kungsbacka (SE). ANDREASSON, Anders,  
Klas [SE/SE]; Traneredsvagen 60A, S-426 77 V Frolunda  
(SE). GOERSMANN, Claus, Friedrich [DE/GB]; 39  
Cromwell Road, Cambridge CB1 3EB (GB). LAVENIUS,  
Mats [SE/SE]; Vandstensvagen 13, S-433 30 Partille (SE).  
TWIGG, Martyn, Vincent [GB/GB]; 108 Ermine Street,

Published:  
— with international search report

[Continued on next page]

(54) Title: SYSTEM AND METHOD OF CONTROLLING REDUCTANT ADDITION



(57) Abstract: An exhaust system (10) for a vehicular lean-burn internal combustion engine (12) comprises a NO<sub>x</sub> reduction catalyst (18), a source of reductant, means (20) for contacting the catalyst (18) with the reductant, means (TC1) for sensing the temperature of the exhaust gas and/or the catalyst bed and means, when in use, for controlling reductant addition, wherein the reductant addition control means supplies an amount of reductant to the catalyst at a rate corresponding to a measured temperature value of the exhaust gas and/or catalyst bed, which temperature value has been pre-determined to correlate, in use, with an amount of NO<sub>x</sub> in the exhaust gas.



— before the expiration of the time limit for amending the claims and to be republished in the event of receipt of amendments

For two-letter codes and other abbreviations, refer to the "Guidance Notes on Codes and Abbreviations" appearing at the beginning of each regular issue of the PCT Gazette.

(88) Date of publication of the International search report:

2 June 2005

# INTERNATIONAL SEARCH REPORT

Inte <sup>nal</sup> Application No  
PCT/GB2004/002643

## A. CLASSIFICATION OF SUBJECT MATTER

IPC 7 F01N3/02 F01N3/20 F01N9/00 F01N11/00

According to International Patent Classification (IPC) or to both national classification and IPC

## B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 7 F01N

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

EPO-Internal, PAJ

## C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	US 6 167 698 B1 (KING EDWARD THOMAS ET AL) 2 January 2001 (2001-01-02)	1,2,17, 18,21, 22,24,25
Y	column 3, line 5 - column 4, line 21; figure 1	17,18
X	US 5 842 341 A (KIBE ET AL) 1 December 1998 (1998-12-01) column 2, line 62 - column 3, line 52; figures 2,3	1,2,21, 24
X	US 6 487 852 B1 (MURPHY KEVIN RICHARD ET AL) 3 December 2002 (2002-12-03)	1,21,24
A	column 3, line 27 - column 5, line 7; figure 1	2
	----- -/--	

☒ Further documents are listed in the continuation of box C.

☒ Patent family members are listed in annex.

\* Special categories of cited documents:

- \*A\* document defining the general state of the art which is not considered to be of particular relevance
- \*E\* earlier document but published on or after the international filing date
- \*L\* document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)
- \*O\* document referring to an oral disclosure, use, exhibition or other means
- \*P\* document published prior to the international filing date but later than the priority date claimed

- \*T\* later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
- \*X\* document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
- \*Y\* document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.
- \*&\* document member of the same patent family

Date of the actual completion of the international search

14 March 2005

Date of mailing of the international search report

29.03.2005

Name and mailing address of the ISA

European Patent Office, P.B. 5818 Patentlaan 2  
NL - 2280 HV Rijswijk  
Tel. (+31-70) 340-2040, Tx. 31 651 epo nl  
Fax: (+31-70) 340-3016

Authorized officer

Zebst, M

# INTERNATIONAL SEARCH REPORT

Int. Patent Application No  
PCT/GB2004/002643

## C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	US 6 119 448 A (EMMERLING GERHARD ET AL) 19 September 2000 (2000-09-19)	1
A	claim 1; figure 1 -----	2
Y	PATENT ABSTRACTS OF JAPAN vol. 2000, no. 01, 31 January 2000 (2000-01-31) & JP 11 270327 A (ISUZU MOTORS LTD), 5 October 1999 (1999-10-05) abstract -----	17,18
A	US 6 415 602 B1 (PATCHETT JOSEPH A ET AL) 9 July 2002 (2002-07-09) column 14, line 61 - column 15, line 42; figure 3 -----	3,4

# INTERNATIONAL SEARCH REPORT

national application No.  
PCT/GB2004/002643

## Box II Observations where certain claims were found unsearchable (Continuation of item 2 of first sheet)

This International Search Report has not been established in respect of certain claims under Article 17(2)(a) for the following reasons:

1. ☐ Claims Nos.:  
because they relate to subject matter not required to be searched by this Authority, namely:
2. ☐ Claims Nos.:  
because they relate to parts of the International Application that do not comply with the prescribed requirements to such an extent that no meaningful International Search can be carried out, specifically:
3. ☐ Claims Nos.:  
because they are dependent claims and are not drafted in accordance with the second and third sentences of Rule 6.4(a).

## Box III Observations where unity of invention is lacking (Continuation of item 3 of first sheet)

This International Searching Authority found multiple inventions in this International application, as follows:

see additional sheet

1. ☐ As all required additional search fees were timely paid by the applicant, this International Search Report covers all searchable claims.
2. ☐ As all searchable claims could be searched without effort justifying an additional fee, this Authority did not invite payment of any additional fee.
3. ☒ As only some of the required additional search fees were timely paid by the applicant, this International Search Report covers only those claims for which fees were paid, specifically claims Nos.:  
1-4, 17-26
4. ☐ No required additional search fees were timely paid by the applicant. Consequently, this International Search Report is restricted to the invention first mentioned in the claims; it is covered by claims Nos.:

Remark on Protest

☐ The additional search fees were accompanied by the applicant's protest.

☒ No protest accompanied the payment of additional search fees.

## INTERNATIONAL SEARCH REPORT

International Application No. PCT/GB2004 /002643

FURTHER INFORMATION CONTINUED FROM PCT/ISA/ 210

This International Searching Authority found multiple (groups of) inventions in this international application, as follows:

1. claims: 1,2,17,18,21-26

System and method of calibrating a rate of reductant addition required to reduce NOx by measuring the temperature value of the exhaust gas and/or catalyst bed and correlating each value with a rate of reductant addition required to reduce NOx to N2 over the NOx reducing catalyst.

---

2. claims: 3,4,19,20

System and method of controlling addition of reductant to a catalyst by providing an oxidation catalyst for oxidising the reductant downstream of the NOx reduction catalyst, measuring the inlet and the outlet temperature of the oxidising catalyst, determining the temperature difference and adjusting the rate of reductant addition so that said temperature difference is within a pre-determined range.

---

3. claims: 5-12

System and method of regenerating a NOx-trap by contacting a fraction of the NOx-trap with a reductant while the NOx-trap as a whole remains in-line to the exhaust gas flow.

---

4. claims: 13-16

System and method of reducing NOx by introducing a reductant at all vehicle speeds in a duty cycle at a rate correlating with a desired NOx conversion at average duty cycle speed and contacting the exhaust gas containing the NOx and the reductant with a NOx reduction catalyst.

---



# INTERNATIONAL SEARCH REPORT

Information on patent family members

International Application No.  
PCT/GB2004/002643

Patent document cited in search report		Publication date	Patent family member(s)	Publication date
US 6167698	B1	02-01-2001	CA 2329090 A1 EP 1111211 A2	21-06-2001 27-06-2001
US 5842341	A	01-12-1998	JP 10047048 A DE 69720883 D1 DE 69720883 T2 EP 0822323 A1	17-02-1998 22-05-2003 11-12-2003 04-02-1998
US 6487852	B1	03-12-2002	DE 10240399 A1 GB 2381762 A	30-04-2003 14-05-2003
US 6119448	A	19-09-2000	DE 19736384 A1 DE 59810976 D1 EP 0898061 A2 TR 9801663 A2	25-02-1999 22-04-2004 24-02-1999 21-06-1999
JP 11270327	A	05-10-1999	NONE	
US 6415602	B1	09-07-2002	AU 9683701 A EP 1339955 A2 JP 2004518053 T WO 0233232 A2 US 2002148220 A1 US 2002152745 A1 US 2002194841 A1 US 2004128982 A1	29-04-2002 03-09-2003 17-06-2004 25-04-2002 17-10-2002 24-10-2002 26-12-2002 08-07-2004